



# Abschlusskonferenz – TP7

Recipe optimization of batch distillation trajectories  
based on a data-driven model



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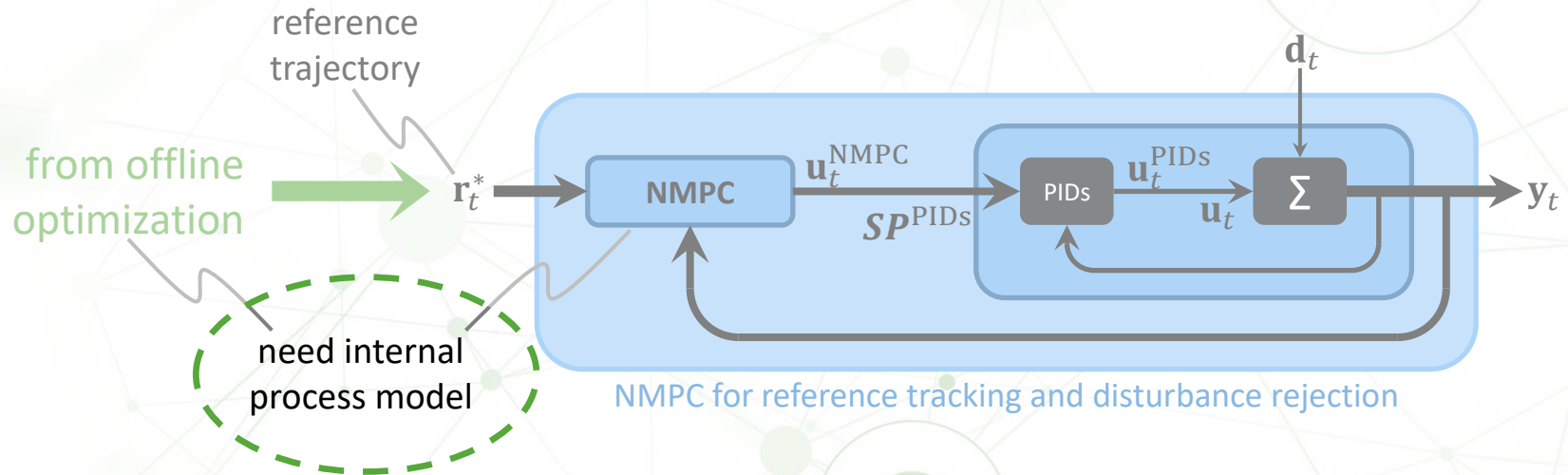


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Erik Esche  
Jens-Uwe Repke



# Goal

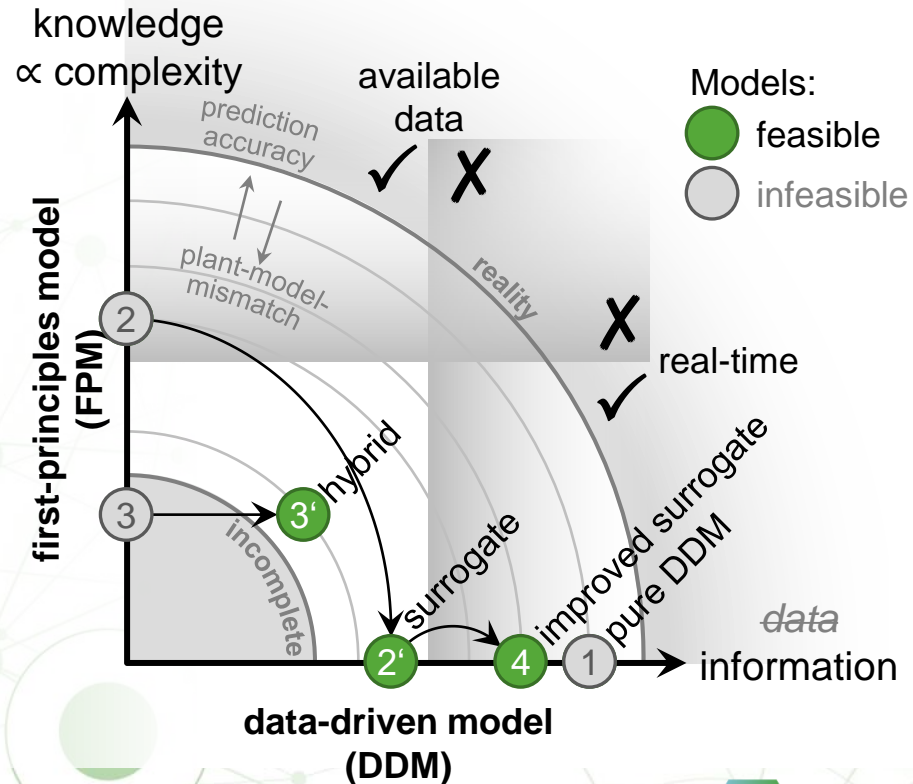
## Optimal operation of batch distillation cycles in an existing plant



# Why data-driven models?

## When are data-driven models (DDM) justified?

1. when no first-principles model (FPM) is available, but real plant data are
  - ideal case, but expensive experiments
2. when the FPM is hard to evaluate or has convergence issues (e.g., large MIMO systems)
  - surrogate DDM for real-time
3. as part of a hybrid (grey-box) model
4. when the FPM is inaccurate, but also little real-plant data are available
  - transfer learning (TL)/domain adaptation



# Case study: Batch distillation

Based on real plant at  **EVONIK**  
Leading Beyond Chemistry

- mixture: methanol + water
- packed vacuum column, fully automated

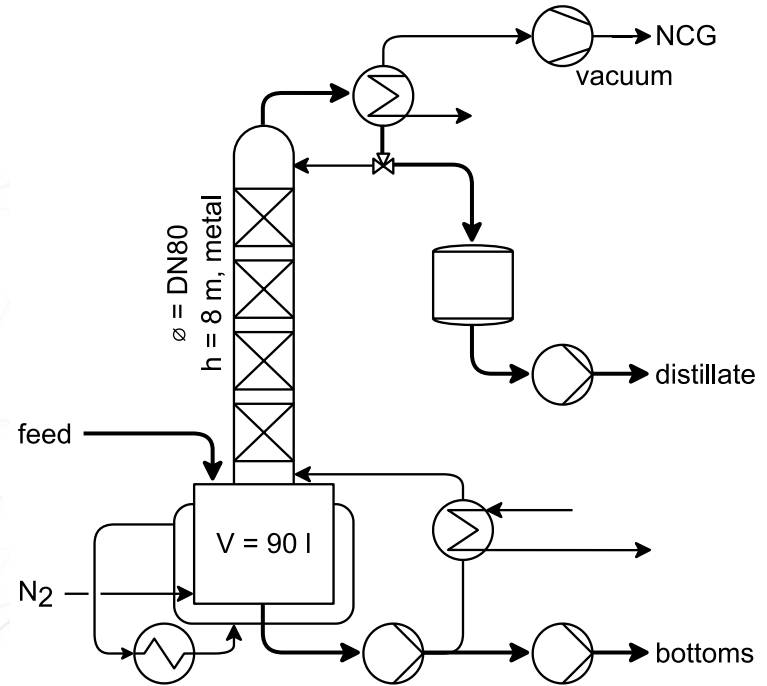
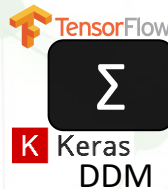
## Simulation (first-principles)

- **pressure-driven**
- **whole batch distillation cycles**
  - from cold and empty startup (inertized at 1 bar)
  - to shutdown (cold and inertized)
- flowsheet simulator: Aspen Plus dynamics



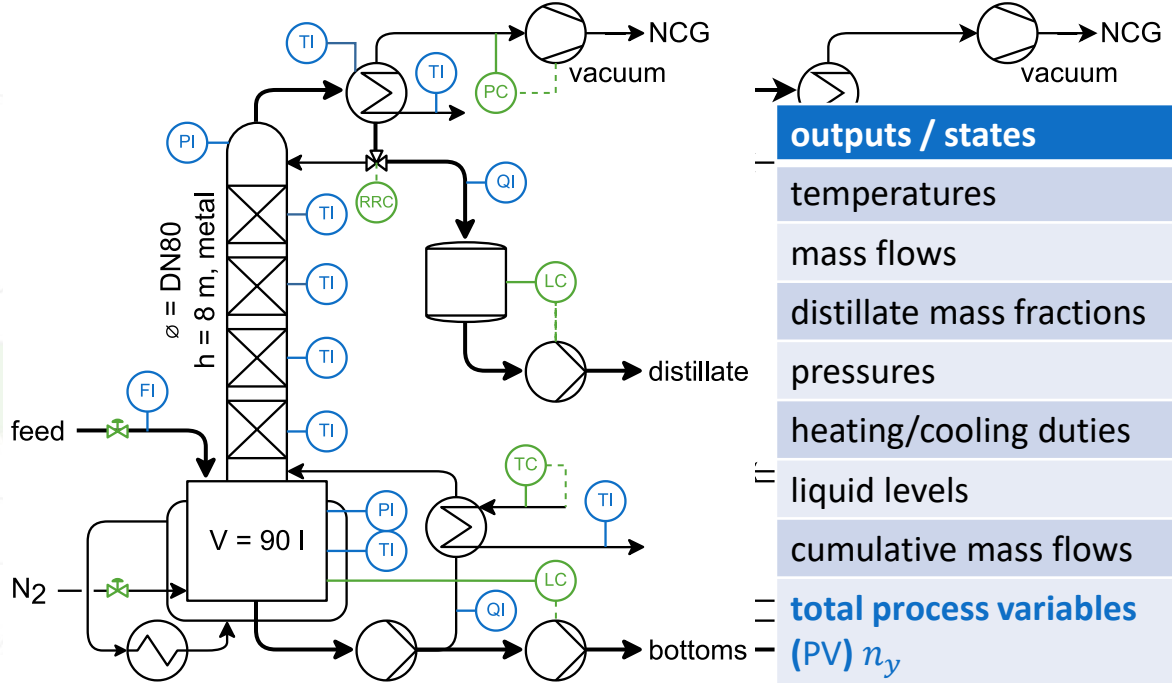
## Data-driven model (DDM)

- large MIMO system
- RNN (2 LSTM layers) in Tensorflow/Keras
  - dynamic
  - long-term dependencies



# Case study: Batch distillation

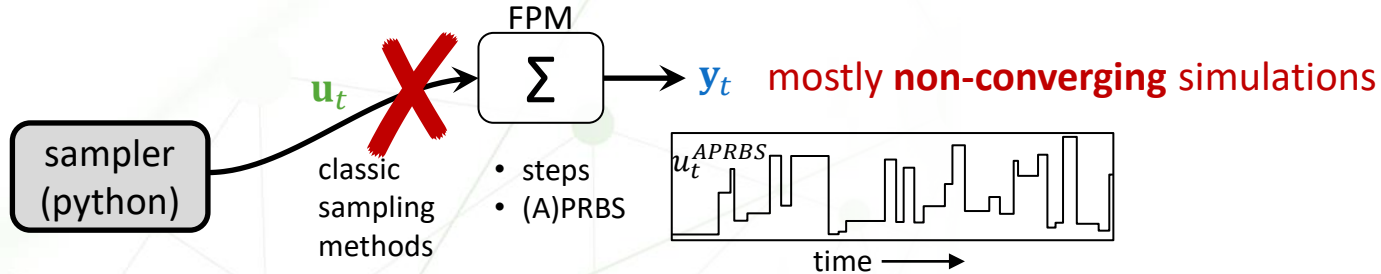
MIMO system



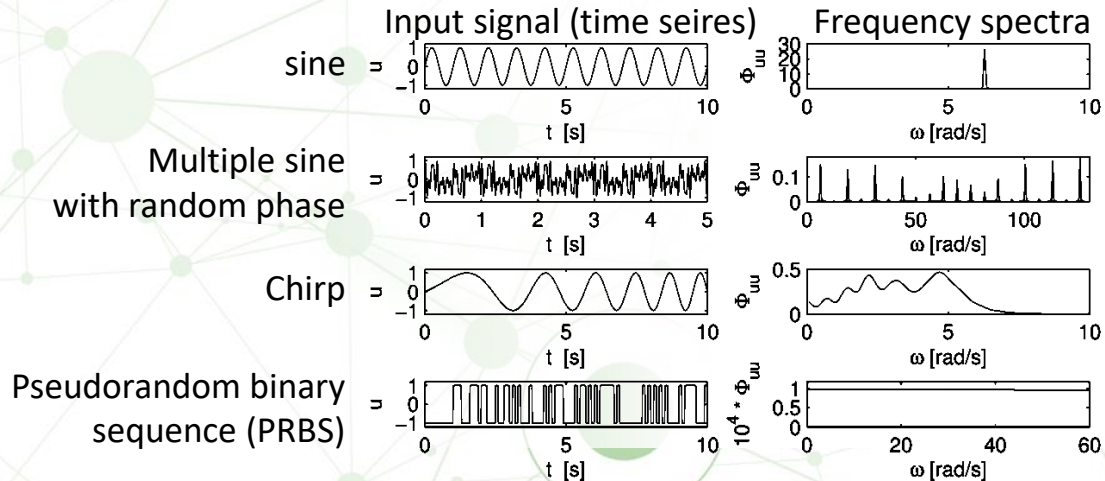
inputs / controls	#
valve positions	2
heating medium temperature	1
reflux ratio	1
controller setpoints (SP)	2
controller modes (AUTO/MAN)	3
<b>total manipulated variables (MV) <math>n_u</math></b>	<b>9</b>

outputs / states	#
temperatures	6
mass flows	6
distillate mass fractions	3
pressures	3
heating/cooling duties	2
liquid levels	4
cumulative mass flows	2
<b>total process variables (PV) <math>n_y</math></b>	<b>26</b>

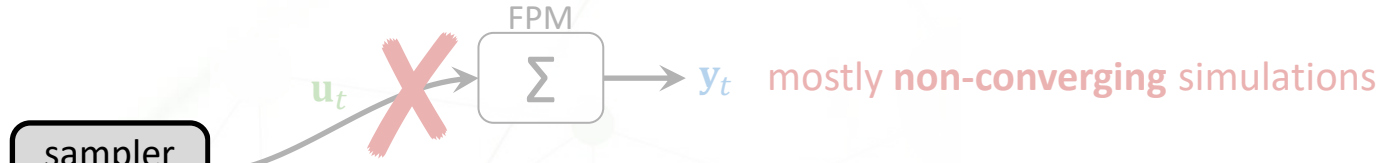
# Dynamic sampling



...and many others



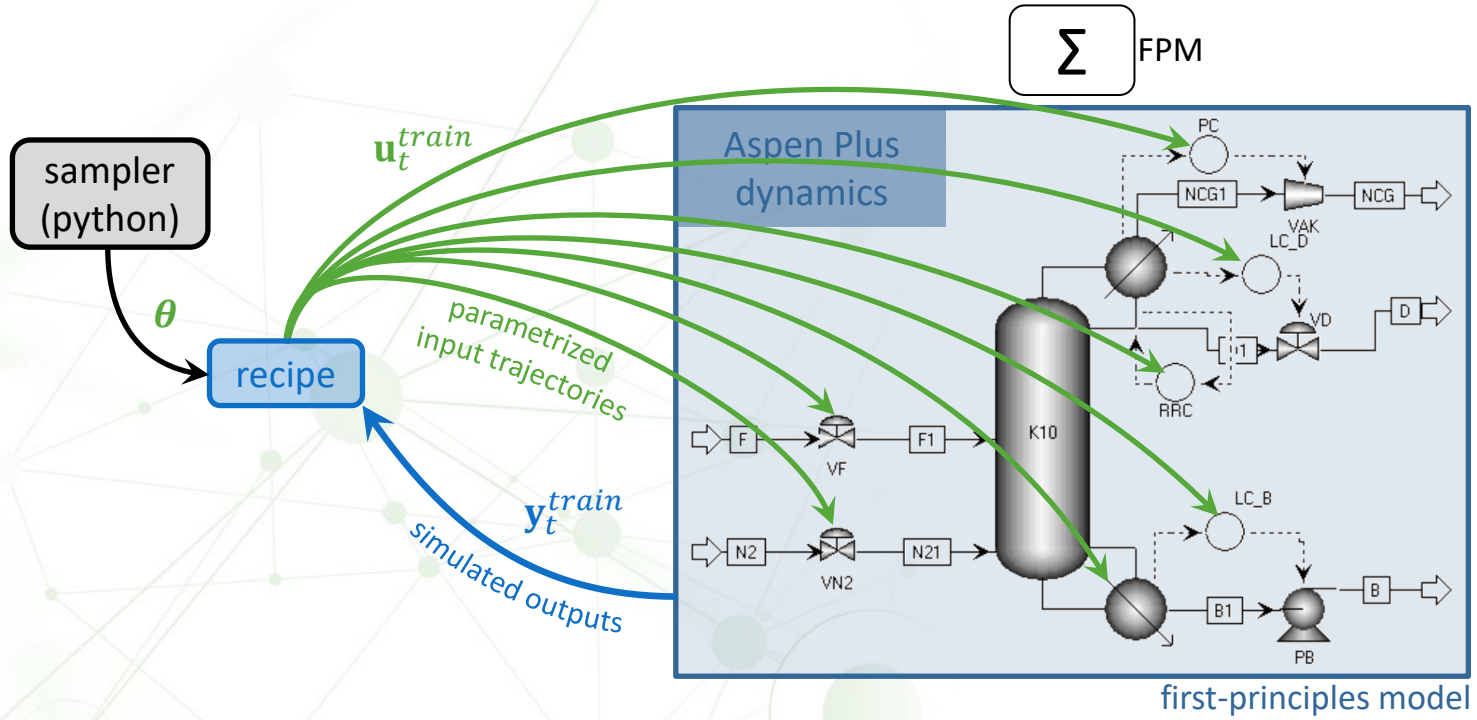
# Recipe sampling



## Recipe for full batch distillation cycle

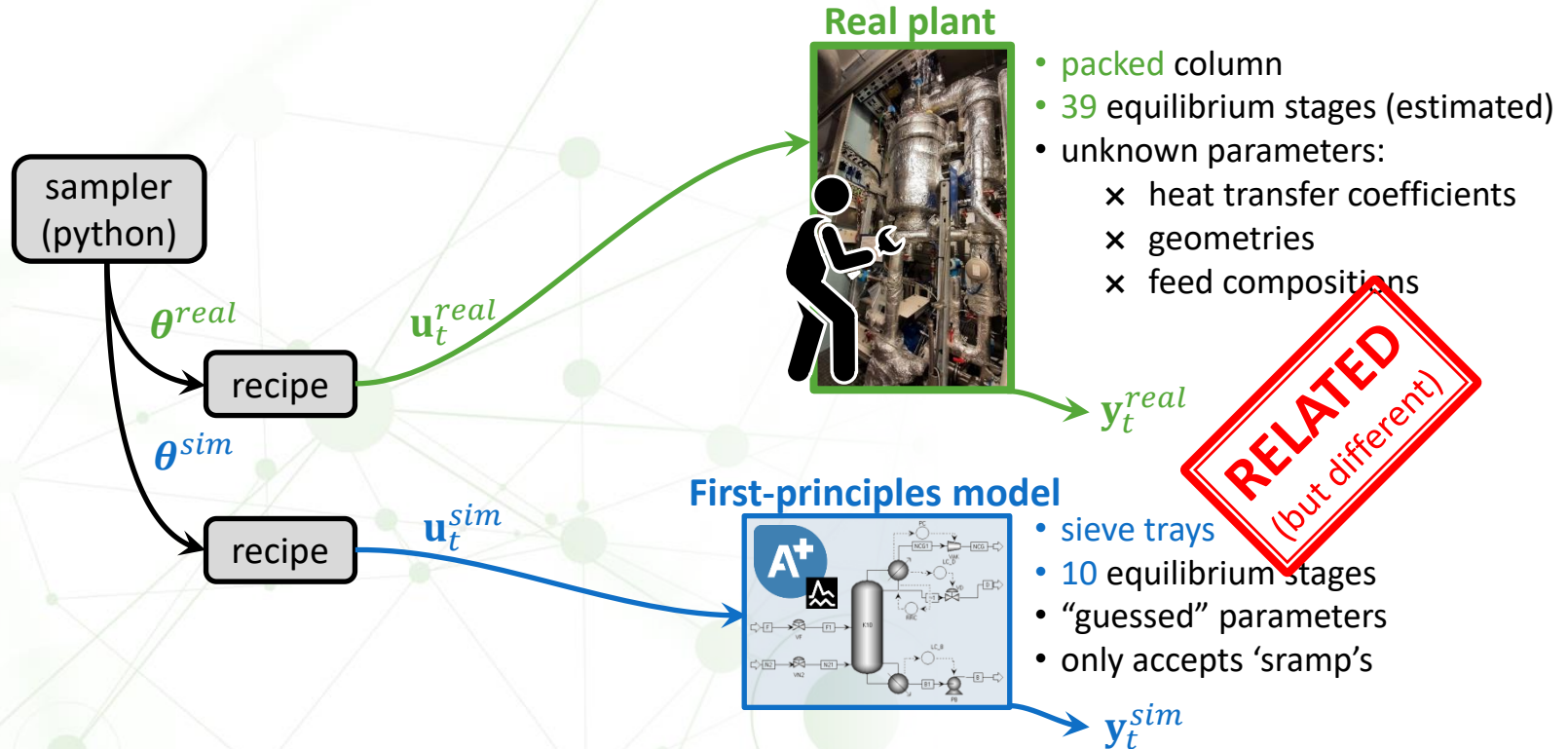
step	description
1	wait for time $\theta_1$ with cold and empty system
:	:
6	heat up reboiler ramping up $T_{med,in}^{Reb}$ to $\theta_7$ during a period of $\theta_8$
:	:
11	wait until achieving a cumulative distillate composition of $\theta_{14}$
:	:

# Recipe sampling



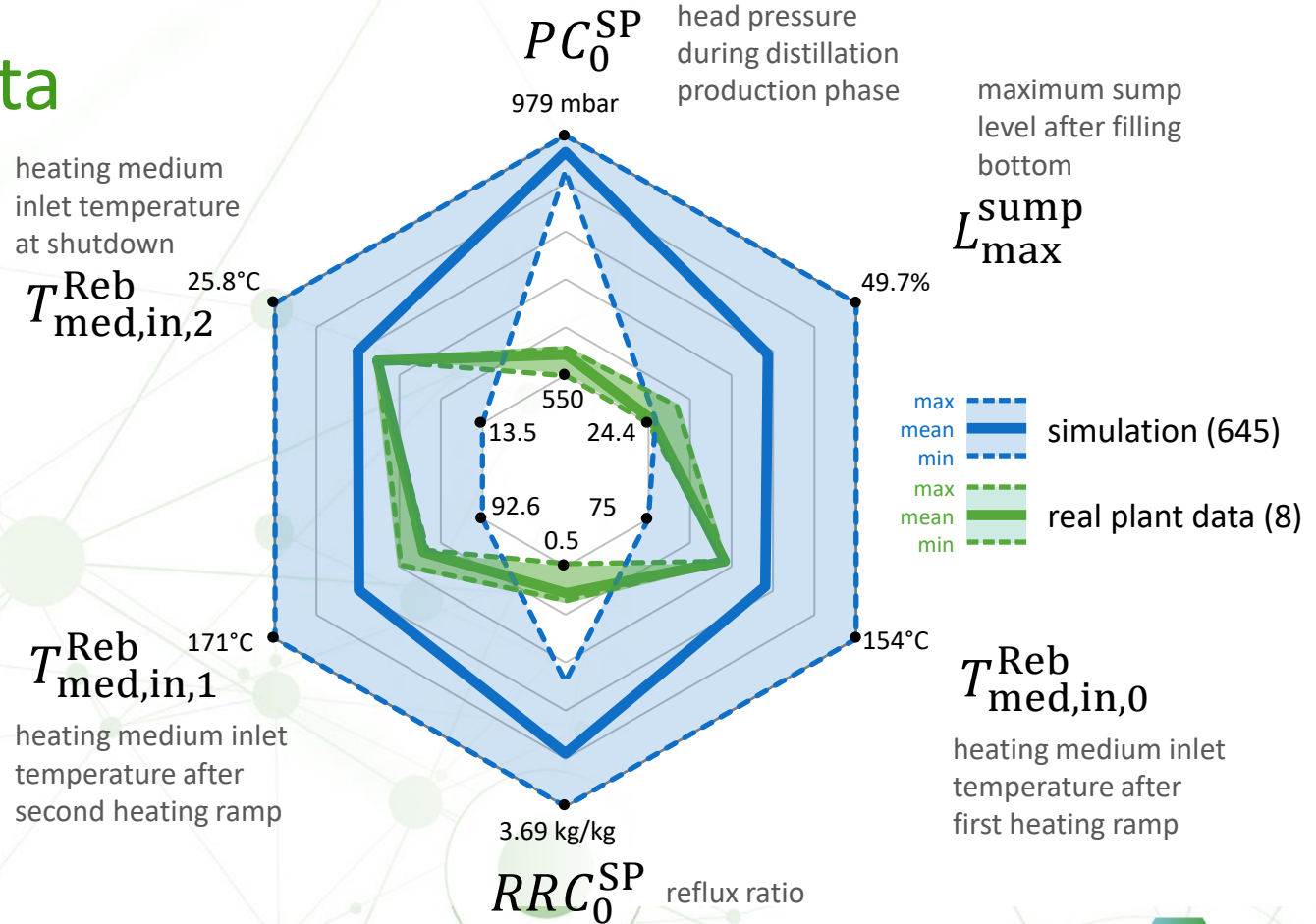


# Dynamic sampling



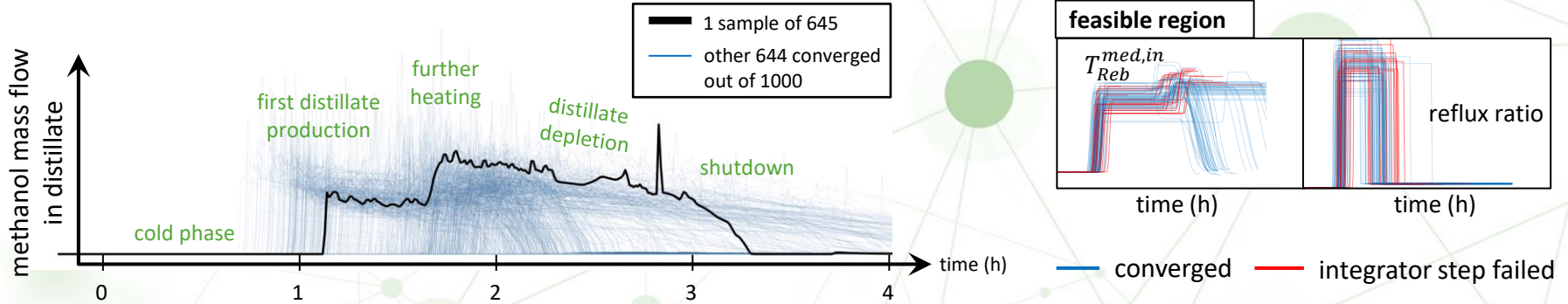
# Available data

6 common (sim, real)  
recipe parameters  
were identified

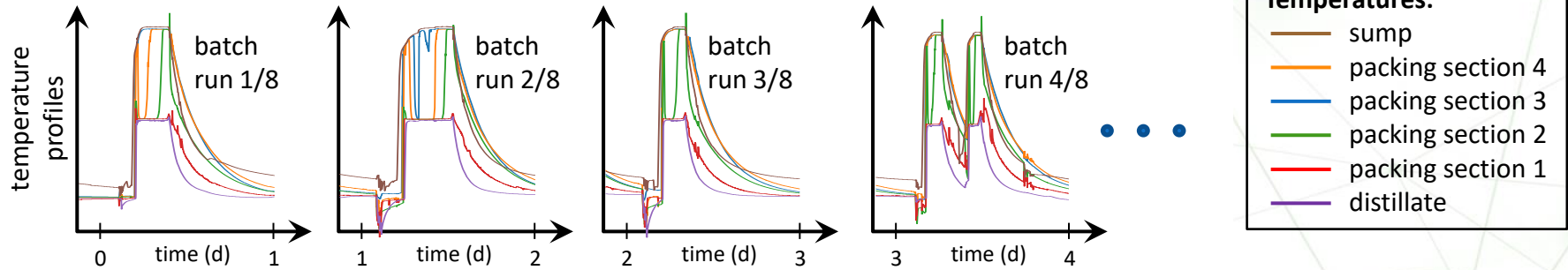


# Datasets

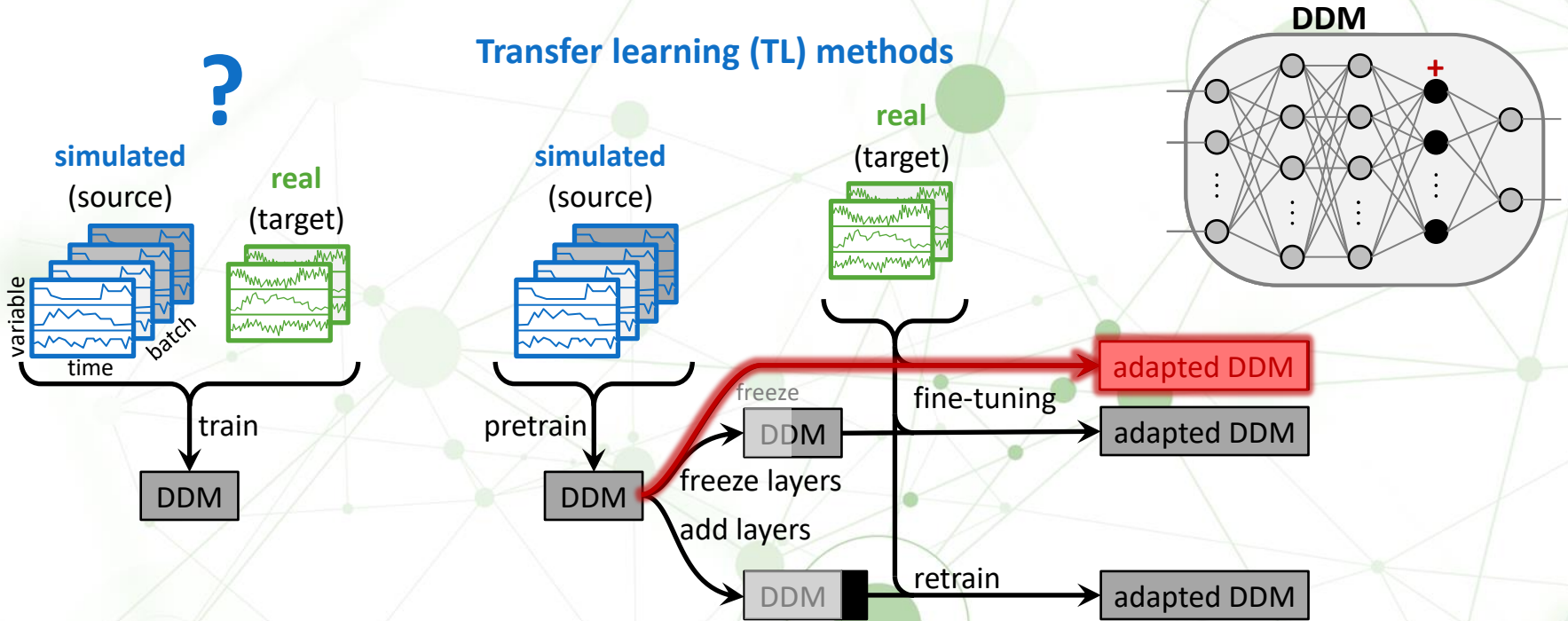
## Simulated data from first-principles model (Aspen Plus Dynamics)



## Real plant data (Evonik/Marl)

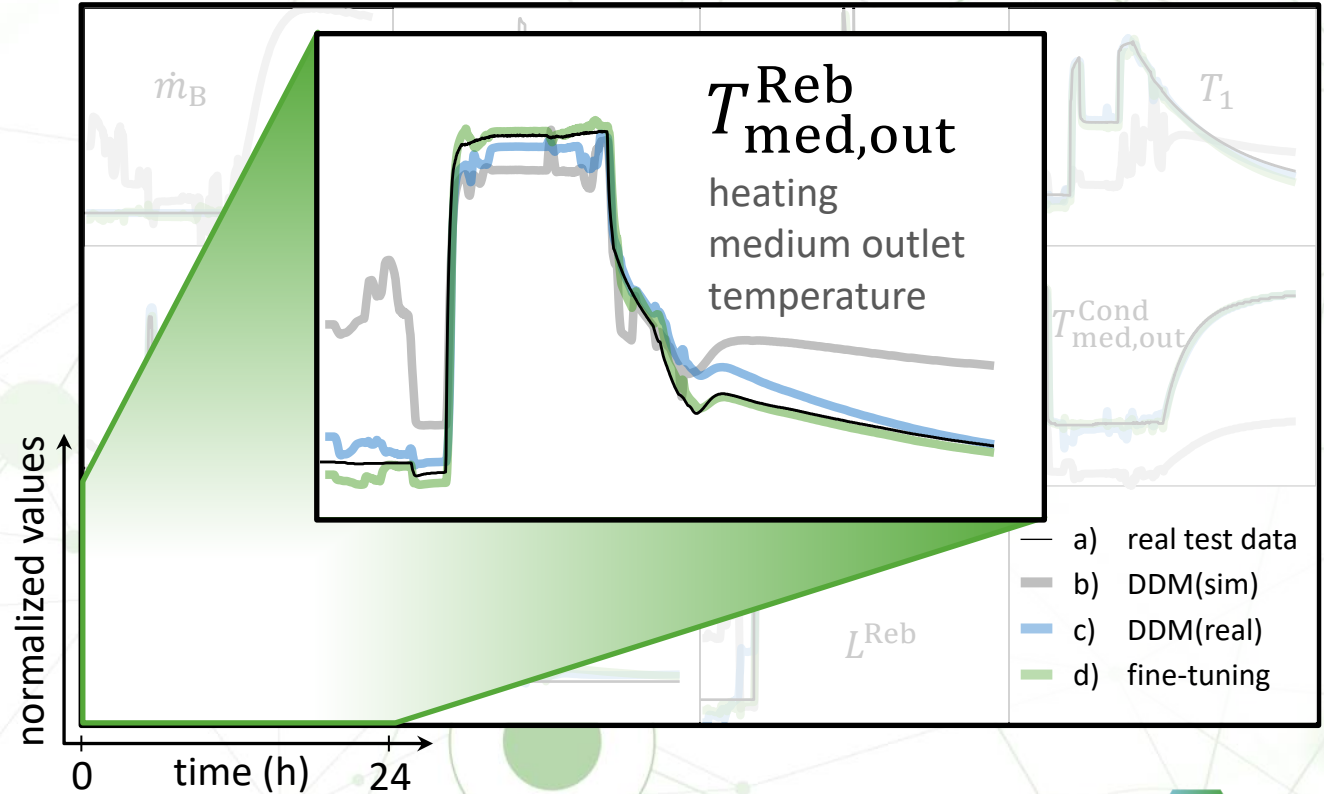
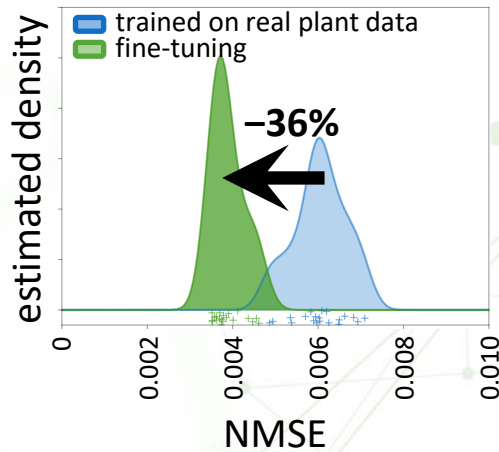


# How to unify both data sources into one model?

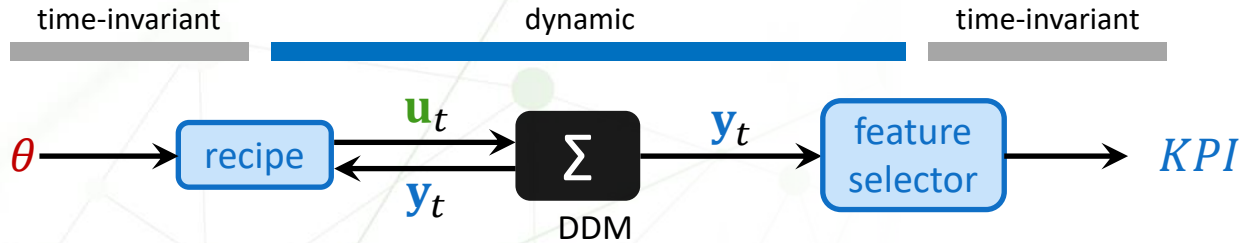


# Test predictions

## Predictions over real plant test data



# Offline optimization options

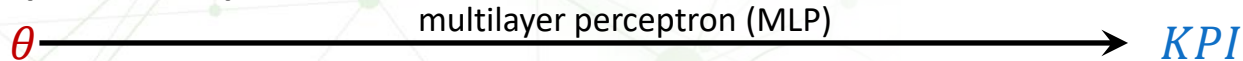


**Optimal control problem (OCP)**



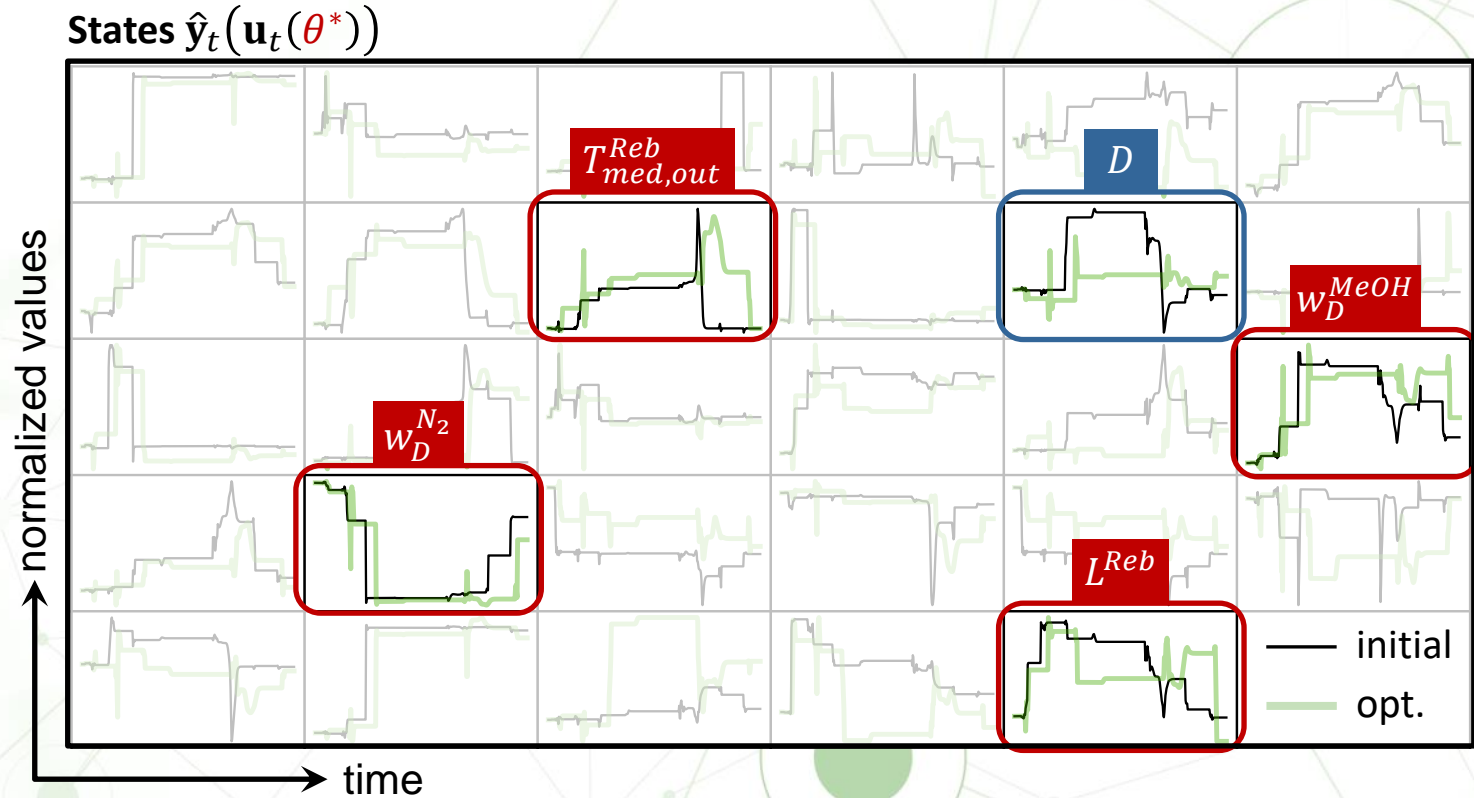
$$\min_{\{u_t\}} f(u_t)$$

**Nonlinear optimization problem (NLP)**

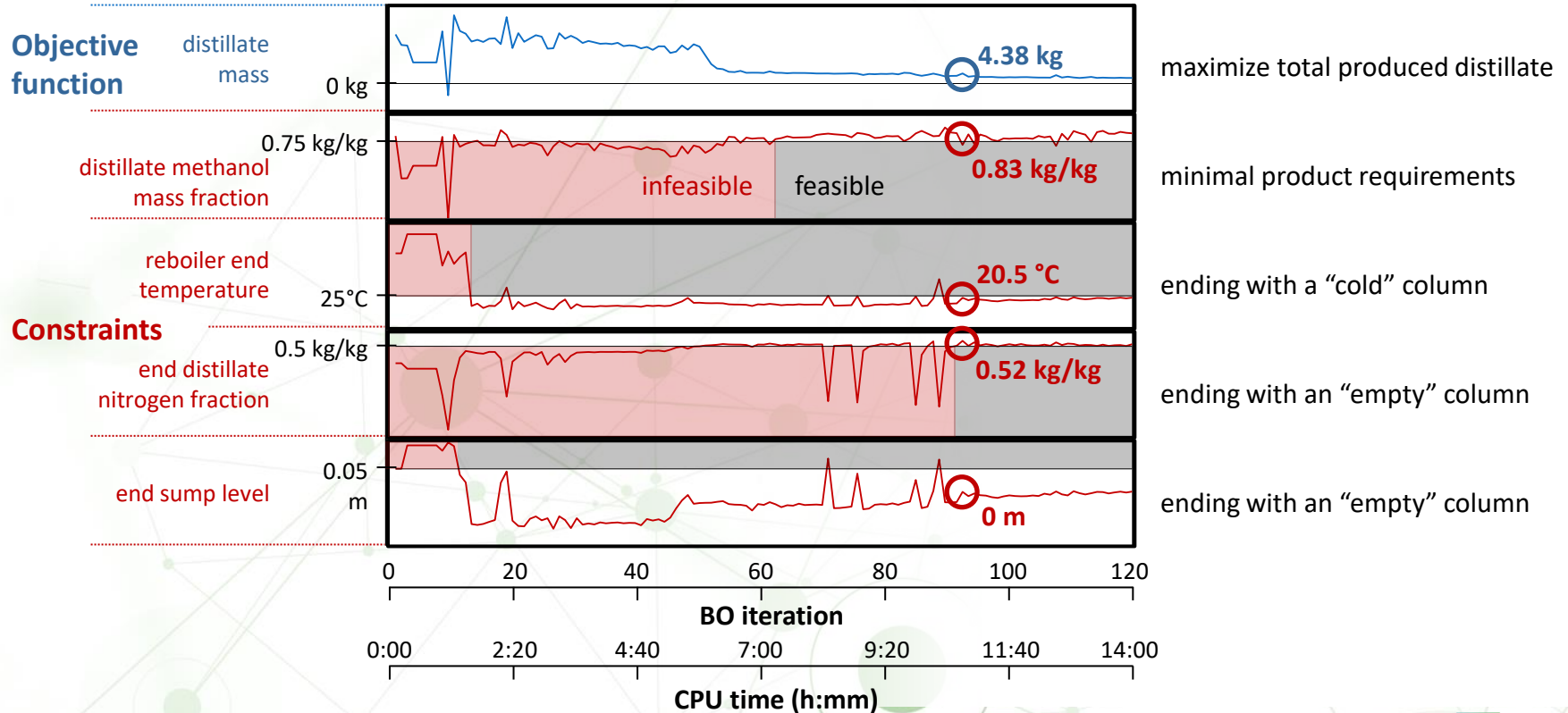


$$\min_{\{\theta\}} f(u_t(\theta))$$

# Optimized trajectories



# Optimization results





# Conclusions

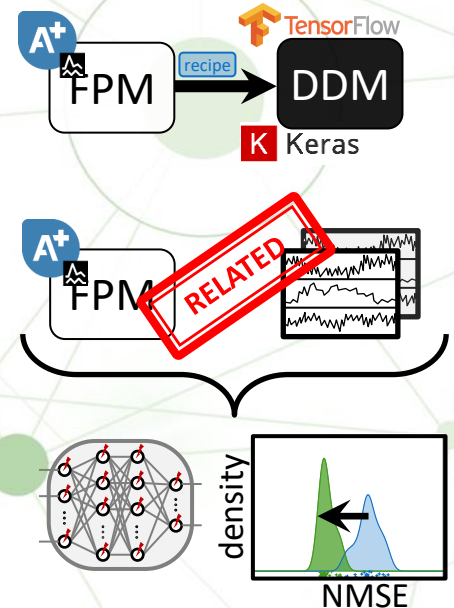
## ➤ Main findings

- a surrogate dynamic data-driven model of a batch distillation could be trained on simulated data from recipe sampling
- scarce real plant data and a related first-principles model can be unified via transfer learning (TL)
- an offline trajectory for a simulated batch distillation column was optimized

## ➤ Outlook

- validation of offline trajectories in the real plant
- use the data-driven model for NMPC

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$$\min_{\{\theta\}} f(\mathbf{u}_t(\theta))$$